MONTANA DEPARTMENT OF ENVIRONMENTAL QUALITY OPERATING PERMIT TECHNICAL REVIEW DOCUMENT

Air, Energy, & Mining Division 1520 E. Sixth Avenue P.O. Box 200901 Helena, Montana 59620-0901

Montana Sulphur & Chemical Company Billings - Lockwood Plant 627 Exxon Road Billings, MT 59107

The following table summarizes the air quality programs testing, monitoring, and reporting requirements applicable to this facility.

Facility Compliance Requirements	Yes	No	Comments	
Source Tests Required	X		Method 5, 6/6C, 9, 7/7E, 11 and 417B	
Ambient Monitoring Required		X		
COMS Required		X		
CEMS Required	X		SO ₂ Concentration in stack gas, stack gas volumetric flowrate monitor	
Schedule of Compliance Required		X		
Annual Compliance Certification and Semiannual Reporting Required	X			
Monthly Reporting Required		X		
Quarterly Reporting Required	X		CEMS, Temperatures, etc.	
Applicable Air Quality Programs				
ARM Subchapter 7 Preconstruction Permitting	X		MAQP #2611-04	
New Source Performance Standards (NSPS)				
National Emission Standards for Hazardous Air Pollutants (NESHAPS)	X		Except for 40 CFR 61, Subpart M	
Maximum Achievable Control Technology (MACT)	X		40 CFR 63, Subpart ZZZZ 40 CFR 63, Subpart CCCCCC 40 CFR 63, Subpart JJJJJJ	
Major New Source Review (NSR)	X		MSCC is defined as a	
Prevention of Significant Deterioration (PSD)	X		major source but has not yet triggered a PSD/NSR.	
Risk Management Plan Required (RMP)		X		

Acid Rain Title IV		X	
Facility Compliance Requirements		No	Comments
Compliance Assurance Monitoring (CAM)		X	
State Implementation Plan (SIP)	X		Billings SO ₂ SIP
Federal Implementation Plan (FIP)	X		Billings/Laurel Area SO ₂ FIP

TRD2611-06 2 Date of Decision: 3/22/2019 Effective Date: 4/23/2019

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SECTION I. GENERAL INFORMATION

A. Purpose

This document establishes the basis for the decisions made regarding the applicable requirements, monitoring plan, and compliance status of emission units affected by the operating permit proposed for this facility. The document is intended for reference during review of the proposed permit by the Environmental Protection Agency (EPA) and the public. It is also intended to provide background information not included in the operating permit and to document issues that may become important during modifications or renewals of the permit. Conclusions in this document are based on information provided in the original application submitted by Montana Sulphur & Chemical Company (MSCC) on June 12, 1996; an additional submittal on March 3, 1999; an administrative amendment request on May 16, 2002; a renewal application submitted February 4, 2005; de minimis requests received on February 23, 2007 and February 29, 2009; an administrative amendment received on July 27, 2009; a renewal application submitted on May 21, 2010 with additional information submitted on August 10, 2010; a renewal application submitted on August 1, 2016, and an administrative amendment request submitted January 24, 2019.

B. Facility Location and Site Description

The MSCC Lockwood facility is located in Yellowstone County, Montana at 627 ExxonMobil Road. The site is a strip of land located in the SE½ of Section 24, Township 1 North, Range 26 East; the NE¼ of Section 25, Township 1 North, Range 26 East; and the SW¼ of Section 19, Township 1 North, Range 27 East. MSCC's plant site is approximately three miles northeast of the city of Billings, at the northeastern end of the Burlington Northern Railroad East Billings industrial switchyard. The greater Billings area lies to the west, with less developed area to the north, south, and east, of the plant. The small, unincorporated community of Lockwood is south of the site.

The facility is located in an area characterized by heavy industrial properties. The plant site is long and narrow, extending approximately one mile along the adjacent Montana Rail Link mainline railroad tracks, generally between Exxon Road and N. Johnson Lane. The Exxon oil refinery and the Exxon RCRA land farm are located adjacent to the northwest property boundary and the Yellowstone Energy Limited Partnership (YELP) cogeneration facility is located to the south. Also adjacent to the southeast boundary of the property are a livestock auction yard, trucking terminals, a carbon dioxide plant, pipeline pumping stations, and a large oil-products terminal.

The Yellowstone River is approximately one-half mile from the facility. Interstate 90 is one-quarter mile to the south of the site. The plant site is generally flat and the elevation is 3107 feet above sea level at the main stack location. Hills and bluffs rise from 3,500 to 3,900 feet and flank the valley to the northwest and southeast. The area has been characterized as rural terrain roughness.

The climate of the area is considered semi-arid. Average rainfall is approximately 13 inches per year with the majority of the precipitation occurring in the late spring and early summer months. The annual temperature is 45 degrees Fahrenheit (°F) with maximum temperatures in the summer ranging from 95 to 100 °F and occasionally exceeding 100 °F. Winter temperatures are typical of continental air masses and can be well below zero at winter extremes.

TRD2611-06 4 Date of Decision: 3/22/2019 Effective Date: 4/23/2019 The air quality classification for the area is "Better than National Standards" or "Unclassified/ Attainment" (40 CFR Part 81.327) for all pollutants near the plant site. There are two small nonattainment areas, for carbon monoxide (CO) and sulfur dioxide (SO₂) within the county. The CO nonattainment area begins in the urban Billings area a few kilometers west of the plant complex. The SO₂ nonattainment area is located around a refinery in Laurel, Montana, approximately 20 miles up-river from the plant site.

C. **Facility Background Information**

Montana Air Quality Permit (MAQP) History

In November of 1977, the Department of Environmental Quality (Department) issued MAQP # 1157 to MSCC, which authorized the construction of a 100-Meter SRU stack at the facility. At that time neither EPA nor the Department had promulgated rules to define Good Engineering Practice (GEP) Stack Height.

Also in November of 1977, the Department entered into a stipulation with several Billings/Laurel industries, including MSCC. The 1977 stipulation, which was in response to an EPA directive, set out control measures for meeting the national standards for SO₂ in the Billings/Laurel area. Paragraph 16 of the 1977 stipulation stated that the MSCC's MAQP 1157 had been issued because "the proposed stack height increases constitute good engineering design." Paragraph 17 of the 1977 stipulation required future permits for stack height increases to be subject to GEP review based upon the 1977 CAA amendments "until such time as the Board adopts a stack height increase rule." The Board first adopted stack height rules in 1978.

By 1981, MSCC had still not constructed its proposed SRU stack. On February 23, 1981, the Department informed MSCC that MAQP 1157 had expired and that a new permit application would be required prior to construction. The expiration of MAQP 1157 was based upon a rule requiring completion of construction within 2-years from the date of issuance (ARM 16-2.14(1)s1400(7). In June of 1981, MSCC attorneys agreed to apply for a new permit, although they sought to retain GEP status for the 100-Meter stack.

MAQP #2611-00

On November 30, 1990, the first MAQP #2611-00 was issued to MSCC. The Department revised its stack height rules in 1983 and 1986 to conform to federal rules. In September of 1989, MSCC applied for MAQP #2611 to build the SRU stack and to modify the existing sulfur recovery operations, which included the construction of the ammonium thiosulfate (ATS) process. Construction of the ATS project was suspended in October 1992 due to litigation initiated by Exxon. With the conclusion of the litigation, MSCC was supposed to proceed with the construction.

MAQP #2611-01

On November 18, 1993, MSCC was issued MAQP #2611-01 to construct and operate the Monaca processing equipment at its sulfur processing plant. The Monaca equipment is designed for the production of supplementary Hydrogen Sulfide (H₂S) for the facility. The Monaca unit is capable of producing about 2 tons per hour of H₂S gas. The gas is then sent to the liquefaction unit.

The addition of the Monaca unit did not increase the amount of liquid H₂S produced since it only provides a different mechanism for providing H₂S gas to the liquefaction unit. MAQP #2611-01 replaced MAQP #2611-00.

MAQP #2611-02

On August 15, 1999, MSCC was issued MAQP #2611-02 to allow MSCC to install a 17million British thermal units per hour (MMBtu/hr) boiler for steam generation and plant heating and to install an additional 35 million british thermal units per hour (MMBtu/hr) incinerator (Incinerator East). The boiler will not debottleneck any process; thus, sulfur production will not increase as a result of the installation of the boiler. The boiler may be vented through the 100-foot (30-Meter Stack), 100-Meter Stack, or its own stack. However, the emissions must be vented to the 100-Meter Stack whenever any fuel (diesel or oils) other than natural gas, or its equivalent in lb/MMBtu of sulfur, is fired in order to preserve the requirements of the Stipulation adopted by the Board of Environmental Review on June 12, 1998 (1998 Stipulation). The incinerator was intended to operate in two different modes. In one mode the incinerator serves as a backup to the current incinerator, while in a second mode the incinerator would serve as a source of sulfur feed to the ATS plant. The air dispersion modeling, performed by MSCC for the Hazardous Air Pollutants (HAPs) emitted from the incinerator, demonstrated compliance with the negligible risk requirement.

In addition, the permitting action allowed MSCC to continue construction of the ATS process equipment and updated the permit with correct rule references and current permit language. Originally, when MAQP #2161 was issued for the ATS process emission limits were established for the ATS equipment and a plant-wide emission limit was included in order to avoid Prevention of Significant Deterioration (PSD) review. The project was not completed by November 30, 1996, and according to MAQP #2161-01 Section V.H, those portions of the permit pertaining to the ATS process were revoked. Therefore, the emission limits established on a plant-wide basis and for the 100-Meter Stack were also rescinded.

On November 13, 1998, MSCC sent a letter to the Department requesting that equipment related to the construction and operation of the ATS operation be retained in the permit. Also, MSCC provided a new Best Available Control Technology (BACT) review for the ATS equipment and stated that they would be preparing a MAQP Application for the incinerator.

MAQP #2161-02 re-established emission limits for the 100-Meter Stack and all associated ATS equipment. The SO₂ emission limit for the 100-Meter Stack was based on the average of the previous 2-years of actual emissions from the 100-Meter Stack plus 39 tons minus the SO₂ emissions from the quench water evaporator treating cooling towers emissions (57.52 tons per year (tpy)).

The former SO₂ limit of 3829 tpy previously established in MAQP #2611 became 3817 tpy. The 21 ton per day (tpd) SO₂ limit for the 100-Meter Stack was removed from the permit because it was based on previous modeling for the 100-Meter Stack, which was conducted at a 65-meter stack height. The limit was previously included to protect the National Ambient Air Quality Standards (NAAQS). Since that time, the 1998 Stipulation incorporated emission limits to protect the NAAQS using a buoyancy flux curve. The limits previously established for the ATS equipment remained the same, with the exception of the plant wide emissions limit.

This limit was been omitted because it was no longer necessary with the new limit established for the 100-Meter Stack. The limits imposed for the 100-Meter Stack and associated equipment were less than those required for PSD review.

The facility's allowable emissions for the boiler and incinerator increased by 2.4 tpy of PM₁₀, 9 tpy of CO, 23.7 tpy of NO_x, 0.4 tpy of SO₂, 0.9 tpy of volatile organic compound (VOC). MAQP #2611-02 replaced MAQP #2611-01.

MAQP #2611-03

On November 23, 2001, the Department received a request from MSCC for approval of a de minimis action that would add an emergency/backup generator to the facility. MSCC submitted modeling and an emissions inventory with the request to confirm applicability under the de minimis rule as well as compliance with ambient air quality standards under the conditions proposed by MSCC. MAQP #2611-03 replaced MAQP #2611-02.

MAQP #2611-04

On February 23, 2007, MSCC submitted a de minimis notification to the Montana Department of Environmental Quality-Air Resources Management Bureau (Department) for SuperClaus Unit #2. Additionally, on February 25, 2009, MSCC submitted a de minimis notification to the Department to install an inert gas system boiler (Cleaver Brooks Boiler) to improve heat recovery.

On May 21, 2010, MSCC submitted a renewal application for their Title V Operating Permit #2611-03. The Department requested additional information on July 19, 2010 and also requested information regarding the status of ATS project. On August 10, 2010, MSCC responded to the Department's request stating that MSCC only constructed the second incinerator and the rest of the process (ATS) was never constructed. Pursuant to Administrative Rules of Montana (ARM) 17.8.762, this portion of the permit would have expired because construction or installation did not commence within the time specified. Therefore, this permit action removes all conditions and applicable references to the ATS unit.

In addition, on July 27, 2010, MSCC requested that the Department update emitting units for clarification to reflect current naming conventions used at the facility. MSCC requested the following:

- Update the mailing address of the facility to 627 ExxonMobil Road;
- Change the name of the redundant incinerator to Incinerator East;
- Change the name of the 100-foot stack to the 30-meter stack;
- Change the name of the existing incinerator to Incinerator West; and
- Change the 35 million British thermal units per hour (MMBtu/hr) Incinerator to Incinerator East.

Additionally, on August 10, 2010, the Department received a de minimis request to add a cooling tower and to replace the boiler treatment lagoon with a boiler blowdown tank. The boiler blowdown tank replaces the 'Boiler Treatment Lagoon with Aeration'.

This system allows water previously routed to the lagoon for percolation and evaporation to be released to the blowdown tank system. According to MSCC, MSCC was required to make this change during renewal of their Montana Pollution Discharge and Elimination System (MPDES) Permit.

In response to the renewal application submitted by MSCC, the Department completed several updates to MSCC's Title V Operating Permit (OP) and this was finalized on January 3, 2012. The operating permit includes conditions of the Federal Implementation Plan for the Billings/Laurel, MT Sulfur Dioxide Area (FIP) and the Stipulated Agreement between the Department and MSCC signed in June of 1998. These conditions exist in the Title V OP, however, MSCC is also required to meet the conditions of the MAQP in addition to the Title V applicable requirements.

In addition to those changes mentioned above, this permit action also updates current language and rule references used by the Department and the emission inventory.

Operating Permit History

Operating Permit #OP2611-00 became effective for facility compliance on July 29, 2000.

Operating Permit #OP2611-01 was an administrative amendment, to changing the responsible official to Larry Zink for the MSCC facility. In addition, the Department updated the general conditions in the permit to more closely reflect current rules and replaced language that "busted" the credible evidence (ARM 17.8, Subchapter 15) rules (namely, by replacing "demonstrate compliance" with "monitor compliance"). Operating Permit #2611-01 replaced Operating Permit #2611-00.

On October 20, 2003, the Department received a request from MSCC for an administrative amendment of Operating Permit #OP2611-01 to update Section V.B.3 of the General Conditions. The amendment incorporated changes to federal Title V rules 40 CFR 70.6(c)(5)(iii)(B) and 70.6(c)(5)(iii)(C) (to be incorporated into Montana's Title V rules at ARM 17.8.12130 regarding Title V annual compliance certifications. Operating Permit **#OP2611-02** replaced Operating Permit #OP2611-01.

On February 4, 2005, the Department received a Title V renewal application from MSCC. Operating Permit #**OP2611-03** replaced Operating Permit OP2979-02.

On February 23, 2007, MSCC submitted a de minimis notification to the Department for SuperClaus Unit #2. Additionally, on February 25, 2009, MSCC submitted a de minimis notification to the Department to install an inert gas system boiler (Cleaver Brooks Boiler) to improve heat recovery.

On April 21, 2008, a Final Rule was published in the federal register for the Federal Implementation Plan (FIP) for the Billings/Laurel, MT Sulfur Dioxide Area. The FIP was a result of EPA's disapproval or partial disapproval of Montana's State Implementation Plan (SIP) on May 2, 2002. Both EPA's disapproval of the SIP and FIP were appealed by MSCC as they relate to their operations. These appeals are currently pending in the Federal Court of Appeals (9th Circuit). Because MSCC is a facility listed in the FIP and the requirements are final, this permit action incorporates requirements of the FIP into the operating permit.

TRD2611-06 8 Effective Date: 4/23/2019 On May 21, 2010, MSCC submitted a renewal application for their Title V Operating Permit **#OP2611-03**. On July 19, 2010, the Department requested additional information for this application and also requested information regarding the status of ATS project.

On August 12, 2010, MSCC responded to the Department's request and stated that MSCC only constructed the second incinerator and the rest of the process (ATS) was never constructed. Pursuant to Administrative Rules of Montana (ARM) 17.8.762, that portion of the permit expired because construction or installation did not commence within the time specified. Therefore, in addition to the renewal, this permit action removes all conditions and applicable references to the ATS unit.

Additionally, this action incorporates the requirements of the FIP. Because the FIP and portions of the SIP have been appealed by MSCC, and any final action remains pending on both the FIP and SIP, MSCC could be subject to several conditions and/or limitations for each emitting unit. However, in most cases, MSCC must comply with the most stringent requirement.

On July 27, 2010, MSCC requested that the Department update emitting units for clarification to reflect current naming conventions used at the facility. MSCC requested the following:

- Update the mailing address of the facility to 627 ExxonMobil Road;
- Change the name of the redundant incinerator to Incinerator East;
- Change the name of the 100-foot stack to the 30-meter stack;
- Change the name of the existing incinerator to Incinerator West; and
- Change the 35 million British thermal units per hour (MMBtu/hr) Redundant or back-up Incinerator to Incinerator East.

On August 10, 2010, the Department received a de minimis request to add a cooling tower and to replace the boiler treatment lagoon with a boiler blowdown tank. The boiler blowdown tank replaced the 'Boiler Treatment Lagoon with Aeration'. This system allows water previously routed to the lagoon for percolation and evaporation to be released to the blowdown tank system. According to MSCC, MSCC was required to make this change during renewal of the Montana Pollution Discharge and Elimination System (MPDES) Permit.

In addition to that mentioned above, this permit action also updated current language and rule references used by the Department. Operating Permit #OP2611-04 replaced Operating Permit OP2611-03.

On August 1, 2016, the Department received a Title V renewal application from MSCC. In the application, MSCC requested that new section be included for the Primary Backup Diesel Compressor Engine, Diesel-Fueled Emergency Backup Engine/Generator, Operation, Loading, and Unloading of Gasoline BOC Storage Tanks, and the Cleaver Books Boiler.

With the addition of the new sections, MSCC requested that IEU17 and IEU18 be removed from the insignificant emitting unit list and be redesignated as significant emitting units because of NSPS requirements.

MSCC also requested that IEU9 be renamed "Small Portable Internal Combustion Engines", IEU13 be renamed "Operation, Loading, and Unloading of Non-gasoline VOC Storage Tanks". MSCC requested the addition of an Adsorber System (IEU17), 65,000 Gallon Amine Storage Bullets (IEU18), Flare Gas System (IEU21), and Flare Gas Total Sulfur Analyzer (IEU22) to the insignificant emitting unit list.

MSCC requested the removal of condition C.15 which relates to backup temperatures and flowrate monitoring within six (6) months after Environmental Protection Agency (EPA) approval of Buoyancy Flux Monitoring Requirements. The EPA did not approve the use of Buoyancy Flux as a means of setting the SO2 emission limit for the facility. Therefore, the condition was now null and void.

Operating Permit #**OP2611-05** replaced Operating Permit OP2611-04.

D. **Current Permit Action**

On February 11, 2019, the Department received an administrative amendment request from MSCC to list three new alternate Responsible Officials for the facility. These three new alternate Responsible Officials are:

Donna Z. Eden, Vice President Samuel PM Gray, Vice President Mark DeHart, Environmental, Health, Safety and Regulatory Manager

As vice presidents, Ms. Eden and Mr. Gray qualify for this designation under ARM 17.8.1201(29)(a)(i). Mr. DeHart was assigned authority and responsibility to sign environmental permit applications, compliance reports, malfunction reports, and other related environmental submittals by the MSCC Board of Directors. Therefore, Mr. DeHart qualifies as an alternate Responsible Official per ARM 17.8.1201(29)(a)(ii). The current action incorporates these individuals into the Operating Permit as alternate Responsible Officials. Operating Permit #OP2611-06 replaces Operating Permit #OP2611-05.

E. Taking and Damaging Analysis

House Bill (HB) 311, the Montana Private Property Assessment Act, requires analysis of every proposed state agency administrative rule, policy, permit condition or permit denial, pertaining to an environmental matter, to determine whether the state action constitutes a taking or damaging of private real property that requires compensation under the Montana or U.S. Constitution. As part of issuing an operating permit, the Department is required to complete a Taking and Damaging Checklist. As required by 2-10-101 through 2-10-105, Montana Code Annotated (MCA), the Department conducted the following private property taking and damaging assessment.

YES	NO	
X		1. Does the action pertain to land or water management or environmental regulation
		affecting private real property or water rights?
	X	2. Does the action result in either a permanent or indefinite physical occupation of private
		property?
	X	3. Does the action deny a fundamental attribute of ownership? (ex.: right to exclude others,
		disposal of property)

YES	NO	
	X	4. Does the action deprive the owner of all economically viable uses of the property?
	X	5. Does the action require a property owner to dedicate a portion of property or to grant an
		easement? [If no, go to (6)].
		5a. Is there a reasonable, specific connection between the government requirement and
		legitimate state interests?
		5b. Is the government requirement roughly proportional to the impact of the proposed use
		of the property?
	X	6. Does the action have a severe impact on the value of the property? (consider economic
		impact, investment-backed expectations, character of government action)
	X	7. Does the action damage the property by causing some physical disturbance with respect
		to the property in excess of that sustained by the public generally?
	X	7a. Is the impact of government action direct, peculiar, and significant?
	X	7b. Has government action resulted in the property becoming practically inaccessible,
		waterlogged or flooded?
	X	7c. Has government action lowered property values by more than 30% and necessitated the
		physical taking of adjacent property or property across a public way from the property in
		question?
	X	Takings or damaging implications? (Taking or damaging implications exist if YES is
		checked in response to question 1 and also to any one or more of the following questions:
		2, 3, 4, 6, 7a, 7b, 7c; or if NO is checked in response to questions 5a or 5b; the shaded areas)

F. Compliance Designation

This facility is inspected annually. The most recent Full Compliance Evaluation was for the time period from August 23, 2016 through December 31, 2018. No violation or warning letters were issued to MSCC, and no formal enforcement actions were initiated by the Department, during this compliance monitoring period.

Date of Decision: 3/22/2019 Effective Date: 4/23/2019

SECTION II. SUMMARY OF EMISSION UNITS

A. **Facility Process Description**

MSCC receives sulfur-containing fuel gases from Exxon, desulfurizes these gases in its amine unit, and returns low-sulfur fuel gas back to the refinery. The other purpose of the facility is to convert the raw sulfur compounds from fuel gases, acid gases, and other materials to create useful, marketable products. With a variety of processes, MSCC creates a multitude of products including elemental sulfur, carbon sulfides, sodium hydrosulfide (NaSH), and dry fertilizers.

Typical operation of the complex consists of treating gases from the refinery using an amine unit. This unit removes the sulfur compounds in the sour gas stream and returns a cleaned fuel gas stream to the refinery. The recovered sulfur compounds are combined with other sulfur-containing gas streams and then primarily sent to the Claus recovery unit (SRU) and converted to elemental sulfur, which is then routed to sulfur storage, shipping, or further processing.

The elemental sulfur produced in the Claus plant may be sold directly or further processed into fertilizer products, animal feed supplements, or industrial sulfur products. Sulfur may be sent to the revised Monaca process to create H₂S or carbon disulfide; however, the three Monaca process emitting units have been idle at the MSCC facility since 1993.

B. Emission Units and Pollution Control Device Identification

EU1 Sulfur Vaporizer Heater and EU2 - Steam Methane Superheater

The Monaca processing equipment is designed for the production of H₂S gas for the facility. The Monaca process has de minimis air emissions. It is designed as a completely enclosed system with the exception of the emissions from two associated heaters, which burn natural gas and/or refinery gas. EU1 Vaporizer Heater is rated at 5.5 MMBtu/hr and it heats raw material sulfur and gases to reaction temperature and also generates steam for the process. EU2 Steam Methane Superheater is rated at 5.0 MMBtu/hr and it pre-heats raw material steam and/or methane for the Monaca process and feeds to the Superheater Unit and directly to the Monaca Reactor equipment. Emissions from the heaters are from the combustion of low-sulfur fuel gas and natural gas; both heaters vent to individual 40-ft stacks.

EU3 100-Meter SRU Stack (Claus, SuperClaus and other units)

The 100-Meter SRU stack handles emissions from the Claus Sulfur Recovery Plant, as well as emissions from the Railroad Boiler, the multipurpose boilers H1, H1A, H1-1, H1-2, and the permitted 17-MMBtu/hr boiler. The Claus Sulfur Recovery Process is a combination of equipment including but not limited to the four boilers listed above, five Claus reactor stages including their associated multi-fuel process re-heaters, process gas coolers, barometric seal legs (which connect to run-down pits discussed elsewhere), and tail gas oxidation heater and oxidation reactor equipment with optional waste heat recovery. A redundant tailgas oxidation heater (Incinerator East) and reactor were permitted by MAQP #2161-02 to allow more continuous operation of tailgas oxidation for odor control.

The original and redundant tail gas oxidizer equipment is designed to operate either catalytically or non-catalytically.

The five Claus reactors are generally configured in a three-stage operation, but may be configured in two-stage operation during reactor maintenance. They are designed to operate as a combined single train or as dual parallel train. By-pass ducting and alternate ducting allow maintenance and operational flexibility over a wide range of operating loads. At reduced loads, the unit has also been configured as a 4-stage Claus plant. Individual reactors and the associated stage equipment may be taken on or off line to allow repairs/maintenance on each stage while operations of the Claus process continue. This is normally accomplished by brief shutdowns to swing blinds on alternate duct routes. Gas is flared during these brief shutdowns. Claus process reheaters are dual fueled, meaning that the reheat energy is provided by either fuel gas or by process acid gas. Normally these are fired by process gases, which join the main Claus process gases at each stage for further processing. The Claus process is capable of converting H₂S rich gases into elemental sulfur by means of partial oxidation and catalytic oxidation-reduction of SO₂ and H₂S. The process also is capable of converting other sulfur containing materials (e.g. carbonyl sulfide, carbon disulfide, mercaptans, sulfuric acid and others) to elemental sulfur in conjunction with H₂S rich feed gases. It is capable of handling small concentrations of volatile ammonia compounds in the acid gas feed. The Claus process is enclosed and pressurized to minimize fugitive emissions and vents to the 100-Meter Stack. Historically, it has vented to the 30-Meter Stack, along with the above boilers, however, Section 3(A)(2)(d) of the STIP prohibits the Claus Process from venting to the 30-Meter Stack. The Claus process is rated at 282 tons per day of elemental sulfur production.

EU4 30-Meter Stack (Boilers and Process Units)

The 30-Meter stack (100-foot stack) may receive emissions from the Railroad Boiler, the Process boilers and the 17-MMBtu/hr boiler in accordance Section 3(A)(2)(d) of the STIP. There are limitations found in the permit and STIP regarding what fuels may be fired in some emission units before being released to the 30-Meter Stack.

EU5 Railroad Boiler

The Railroad Boiler's maximum rated design capacity is 18-MMBtu/hr and it was manufactured in 1904. It is primarily fueled with fuel gas or natural gas and operates year round. The boiler also has an oil/liquid fuel firing capability, which is used intermittently and rarely. The liquid firing capability is used primarily to recover heating value from spent lubricants, non-chlorinated solvents, glycols, and alcohols generated incidental to the company's on-site operations. The Railroad Boiler can vent through its own stack (43 feet), the 30-Meter Stack, or the 100-Meter Stack.

EU6 Fuel Gas Boiler H-1 and EU7 Fuel Gas Boiler H1-A

Fuel Gas Boilers H1 and H1-A are multipurpose units that can serve as auxiliary steam generators (variable Btu fuel gas-fired) or as a component in the Claus unit. The boilers were manufactured in 1959 and have Bigelow boiler ratings of 19-MMBtu/hr; this is a minimal design or performance rating not a maximum rated design capacity and may understate the capacity by 15% or more.

When configured as part of the Claus unit, the boilers separate stacks are closed and emissions are vented through the 100-Meter Stack. When configured as fuel-fired steam generators, each boiler vents emission through its own 27-foot stack or the 30-Meter Stack. Flue gas emissions from these boilers, when fueled by fuel gas or natural gas may be partially diverted as feed to the Inert Gas Unit. In either "fuel burning" or Claus service, this multipurpose boiler is designed with a burner that allows combustion of gases from hydrogen to LPG and substantial amounts of entrained liquids (e.g., distillates, water) in liquid/gas mixtures.

EU8 Fuel Gas Boiler H1-1 and EU9 Fuel Gas Boiler H1-2

Both boilers serve the same functions as fuel gas boilers H1 and H1-A so their process descriptions will not be repeated. Fuel Gas Boiler H1-1 was manufactured in 1956 and Fuel Gas Boiler H1-2 was manufactured in 1963. Their Bigelow ratings are both 13-MMBtu/hr that may be understated by 15% or more. These boilers may vent to the 100-Meter Stack at any time or, when not in Claus service, may be vented through the 30-Meter Stack, or may vent to its own stack. Fuel Gas Boiler H1-1 has a 38-foot stack and Fuel Gas Boiler H1-2 has a 23-foot stack.

EU10 17-MMBtu/hr Boiler

The 17-MMBtu/hr boiler was constructed by York-Shipley in 1981. The primary purpose of the boiler will be for steam generation and plant heating. It has the capability of firing gas, diesel, used oil, and residual oil and may, in the future, augment or replace the Railroad Boiler. The boiler can vent through its own stack (43 feet) or the 30-Meter Stack when fired on natural gas, or to the 100-Meter-Stack at any time or when fired on fuels other than natural gas.

EU11 Incinerator East and EU11a Incinerator West

The Incinerator West was installed prior to 1968 and was grandfathered from permitting. The only requirements for this incinerator are those imposed by rules (e.g., Opacity).

Incinerator East serves as a backup to the Incinerator West. It is contemplated that this incinerator will be used primarily when the main incinerator needs to be taken off-line for repairs and the like. There could be brief periods when both incinerators operate at the same time. One example is when one unit is being brought up while the other is being taken off-line for servicing.

EU12 80-foot West Flare (west of the 100-meter stack), EU13 125-foot East Flare (near Monaca Process), and EU14 100- Meter West Flare (located on 100-Meter SRU Stack)

Occasionally during operation, off-specification gases are received from the refineries or upstream units and sent directly to a flare to prevent damage to the operating equipment and hazard to persons. Pressure relieving devices are also connected to the flares. In addition, normal activities incident to the operation and maintenance of the facility direct some routine emissions to the flares, including without limitation purging of vessels and piping incident to plant and transportation equipment testing and maintenance, disposition of excess hydrogen and fuel gas materials, disposition of hydrocarbon rich streams from

portions of the NaSH process, startup/shutdown activities involving acid gases, and similar activities. There are three flares at the facility, one 80-foot West Flare, one located on the 100-Meter Main Stack, and the other 125-foot East Flare, located near the Monaca Process area. The flares have as part of their design continuous pilot lights burning natural gas, lowsulfur fuel gas, or LP Gas to assure ignition of any flows to these flares.

EU15 Hydrogen Plant

Hydrogen may be produced in a 3-step process in the existing plant. Steam and preheated natural gas (or other suitable desulfurized lighter hydrocarbons) are sent to a gas fired reformer unit, producing crude hydrogen over a catalyst. CO produced in the reformer unit is converted to carbon dioxide (CO₂) and hydrogen using a shift converter and a fixed catalyst bed. A carbon dioxide removal unit returns a hydrogen gas stream, normally about 99.9% pure. The separated non-hydrogen-rich stream is sent to a burner unit for combustion as fuel. Product hydrogen is available for use on-site (e.g., Monaca Unit) or for sale to others.

EU16 Liquid Hydrogen Sulfide (H₂S) and Compressor Unit

The Liquid H₂S and Compressor Unit processes acid gases (raw H₂S) into a purified stream of H₂S and streams enriched in light gases (e.g. carbon dioxide, methane, ethane, propane, nitrogen) and enriched in 'heavy' vapors (e.g. butanes and heavier, water, carbon disulfide, ammonia), which in turn are processed in the Claus Unit or other processes on site. Feed for this unit is diverted from Claus Feed and may arise, for example, from the Amine Unit or the Monaca Unit. To the extent H₂S is not returned to the Claus Process this unit also serves to reduce overall SO₂ emissions from the facility. The purified H₂S is stored in pressurized storage on site and loaded into pressure vessels for shipment (e.g. railcars, highway trailers, and cylinders). Excess purified H₂S is also processed into elemental sulfur or NaSH. During periods of startup, shutdown, malfunctions, etc. emissions from this unit are vented to the flare(s) to the extent they are not accommodated in the Claus process. Production of liquid H₂S is limited to 82 tons per day in MAQP #2611-03. Acid gases in the liquid H₂S unit are compressed. Seals on these compressors are purged with fuel gases (e.g. natural gas, methane) to prevent accumulation of H₂S or its escape to atmosphere in large quantities. Purge gas is vented to the flares or to the Claus Tailgas Oxidizer where oxidation to CO₂ and SO₂ occurs. The crankcases of each of these specialized compressors are airpurged to prevent accumulation of gases therein arising from fugitive mechanical seal leakage. The purge air is vented to atmosphere for safety and may contain small quantities of H₂S or VOC's.

EU17 Molten Sulfur Storage

The molten sulfur is stored in enclosed above ground storage tankage with small atmospheric vents. Emissions are considered to be volatile sulfur vapors/gases, resulting from the evaporation and cooling of the elemental liquid sulfur and releases of small amounts of SO₂ and H₂S that may be dissolved in the sulfur in low concentrations. The formation of SO₂ in the air directly surrounding the vent from sulfur vapor is not likely absent combustion.

EU17a Molten Sulfur Storage in Railcars and Mobile Tanks

Molten sulfur is also stored in rail tank cars and other mobile tanks after loading. Individual tanks hold less than 210,000 pounds of sulfur. The molten sulfur is stored in enclosed above ground storage tankage with a small atmospheric venting. Emissions from the tanks are considered to be volatile sulfur vapors/gases, resultant of the evaporation and cooling of the elemental sulfur and release of small amounts of SO₂ and H₂S that may be dissolved in the sulfur in low concentrations.

EU18 Molten Sulfur Loadout/Unloading

The molten sulfur can be loaded directly into either railcar tanks or over-the-road tanker trucks through a top opening on each tank. Molten sulfur is also unloaded in rail tank cars and other mobile tanks. Individual tanks hold less than 210,000 pounds of sulfur. Steam coils may be used to heat the tanks during unloading. Emissions from the tanks are considered to be volatile sulfur vapors/gases, resultant of the evaporation and cooling or heating of the elemental sulfur and releases of small amounts of SO₂ and H₂S that may be dissolved in the sulfur in low concentrations. The formation of SO₂ in the air directly surrounding the vents from sulfur vapor is not likely absent combustion.

EU19 Molten Sulfur Run-down Pits

As liquid sulfur is recovered in the Claus Process including the boilers in Claus service, it passes through barometric seal legs that serve to keep the pressurized process gases inside the Claus unit. These seal legs discharge the separated molten sulfur into small open rundown pits at the base of the unit en route to underground holding reservoirs also called rundown pits. The run-down pits are small and vent to atmosphere. Emissions from the rundown are considered to be volatile sulfur vapors/gases, resulting from the evaporation and cooling or heating of the elemental sulfur and releases of small amounts of SO₂ and of H₂S that may be dissolved in the sulfur in low concentrations. The fresh sulfur is also partially air-stripped by injection of compressed air in the larger underground reservoirs. The formation of SO₂ in the air directly surrounding the vents from sulfur vapor is not likely absent combustion release.

EU20 Sulfur and Fertilizer Manufacture, Conveying and Loadout

Fertilizer is produced on-site by mixing the sulfur with bentonite clays, and processing the mixture to form fertilizer pellets, pastilles, prills, flakes or slates. The material is sized and may be crushed as part of the process depending on end use. The finished fertilizer product can be loaded into bags of various sizes for sale or storage, or can be directly loaded into an over-the-road truck or railcar for transport. Possible emission sources for the process are the open mixing of the sulfur and clay, the forming machinery, the conveying, recycling and/or crushing of the fertilizer pellets, and the loadout of the fertilizer product. The sulfur and clay are mixed in vessels with partially open tops and/or vents with a possibility of volatile sulfur emissions and minimal clay particulate emissions. The forming machinery and the rooms containing it are positively vented to outdoors. The fertilizer pellet conveyors, treaters and sizing equipment in portions of the process are enclosed or covered and have a continuous layer of inert gas applied to limit dust and minimize the possibility of dust explosions. The inert gas - blanketed equipment is maintained at a slight positive pressure.

Product is discharged from blanketed areas through airlock arrangements or by use of product seals. Inert gas lost as fugitive emissions from flanges and connections is replaced continuously as needed. Re-melting in steam heated, open melters recycles unwanted sizes. Particulate emissions (PM₁₀) from the manufacture of pellets are generally limited to the claymixing tanks and the transfer points between conveyors, fugitive emissions, and the recycle and loadout transfer points.

EU21 Sulfur Product Manufacture, Conveying and Loadout

The molten sulfur can be processed on-site to produce several varieties of solid sulfur flakes, slates, powders, and granules. After forming, the products may be ground, sized, and/or recycled. The high purity finished sulfur products can be loaded into bags of various size for sale or storage, or can be directly loaded into over-the road trucks for transport. Possible emission sources for the process are the conveying and loadout of the sulfur products, the discharges of recycle streams to remelt, and fugitive emissions. The sulfur product conveyors, grinders, and sizers in portions of the process are covered and have a continuous layer of inert gas applied to limit dust and minimize the possibility of explosions. A slight positive pressure of inert gas is maintained in the equipment by the inert gas generator equipment. Airlock equipment or product seals are used at discharge points. Inert gas is replaced as needed from the inert gas equipment as it escapes as fugitive emissions. The SO₂ content of the inert gas is considered insignificant. Open melters recycle unwanted sizes. The forming operations and the rooms where these operations occur are positively ventilated to atmosphere. Emissions from the remelt operations and forming operations are expected to be sulfur vapors, as discussed above for handling molten sulfur. SO₂ emissions are expected to be minimal absent combustion. Emissions from the manufacture of the solid sulfur products are generally limited to the transfer points between conveyors, discharge to recycles points, fugitive emissions and the loadout transfer points.

EU22 Various Valves, Pumps and Flanges Leaks

Process equipment used in the production of desulfurized fuel gas; hydrogen, H₂S, sulfur and associated products have numerous valves, pumps, and flanges, all with the potential to release emissions to the atmosphere. Valves include manual and control valves, with packing and numerous pressure safety relief valves. Some pressure relief valves vent to the flare(s) and others vent to the atmosphere. Pumps include liquid and gas pumps and compressors. There are numerous pipes interconnecting the complex equipment in the facility with flanged connections and access to the process vessels, heat exchangers, boilers, and related equipment. Depending on the contents of the piping or vessel the nature of the potential or actual emissions from each of these thousands of points will vary but generally will reflect the contents of the specific system. Thus, fugitive emissions from the fuel system, hydrogen plant, hydrogen permeation equipment etc. may contain methane and hydrogen, along with lesser concentrations of VOC's and H₂S. For example, fugitive emissions from the acid gas handling equipment, NaSH equipment etc. similarly would be expected to contain H₂S and lesser concentrations of VOC's. Fugitive emissions from the Claus process equipment generally would be expected to contain H₂S, SO₂, sulfur vapors, CO, and lesser amounts of carbonyl sulfide and carbon disulfide. Molten sulfur lines, which run throughout much of the facility may release sulfur vapors and small amounts of H₂S and SO₂ associated with the sulfur.

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Because of the extensive nature of the piping, vessels, and other equipment in the facility as a whole and the fact that no reliable means of quantifying these emissions was identified, the collective emissions are estimated to be significant.

EU23 Fugitive Emissions - Access Roads

These emissions are a result of vehicle travel on paved and unpaved portions of the facility. MSCC estimates that 65% percent of the access roads are paved and 35% are unpaved.

EU24 Primary Backup Diesel Compressor Engine – EU25 Diesel-Fueled Emergency Backup Engine/Generator

The primary backup diesel compressor engine is a 1,100 horsepower, trailer mounted, dieselfired internal compression engine used as a power source in the event that mainline power is interrupted.

The primary backup diesel compressor engine provides backup air pressure to the facility during power outages and when primary electric compressors are otherwise unavailable.

EU26 Operation, Loading, and Unloading of Gasoline VOC Storage Tanks

This emitting unit consists of two tanks, each with a gross size of approximately 285 gallons that are used to receive, dispense, and store gasoline. Emissions resulting from operation, loading, and unloading of gasoline VOC storage tanks losses are the primary source of evaporative emissions from tank truck operations. Loading losses occur as organic vapors in "empty" cargo tanks are displaced to the atmosphere by the liquid being loaded into the tanks. These vapors are a composite of (1) vapors formed in the empty tank by evaporation of residual product from previous loads, (2) vapors transferred to the tank in vapor balance systems as product is being unloaded, and (3) vapors generated in the tank as the new product is being loaded.

EU27 Cleaver Brooks Boiler

The Cleaver Books Boiler generates inert gasses used for explosion and fire suppression, primarily in the fertilizer plant. A portion of its flue gas is conditioned and compressed in the adjacent inert gas equipment which serves the sulfur and fertilizer plant and elsewhere in the facility.

C. Categorically Insignificant Sources/Activities

MSCC identified several emission units as insignificant in their permit application (June 12, 1996). However, what was identified in the application as insignificant and what the Department has actually identified as insignificant differs as a result of a March 31, 1998, rule change. This list was also updated by MSCC during the renewal application received on May 21, 2010.

Insignificant emission units were previously defined as any activity or emissions unit located within a source that has a potential to emit less than 5 tpy of any pollutant, does not have the potential to emit hazardous air pollutants in any amount, and is not regulated by an applicable requirement.

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Under the new definition an insignificant emissions source must have the potential to emit of less than 5 tpy of any regulated pollutant, a potential to emit less than 500 lbs. of any HAP, and must be regulated by an applicable requirement other than those generally applicable requirements that apply to all emission units (e.g., opacity, process weight, sulfur in fuel etc.). The insignificant emission units have been identified in Appendix A of the permit.

EU ID	Description	
IEU1	Amine Unit	
IEU2	NaSH Plant, Atmospheric NaSH Plant Storage, Atmospheric NaSH and Caustic Loading/Unloading	
IEU3	Inert Gas Units (2)	
IEU4	Hydrogen Permeation Unit	
IEU5	Cryogenic Storage	
IEU6	Solid Sulfur Storage, Handling and Loadout	
IEU7	Sulfur Scrap Handling and Remelt	
IEU8	Gasoline fueled, Emergency/Back-up Generator	
IEU9	Small Portable Internal Combustion Engines	
IEU10	Repair and Maintenance Activities	
IEU11	Space Heaters < 500 MBtu/hr	
IEU12	Welding/Grinding/Cutting Operations	
IEU13	Operation, Loading, and Unloading of Non-Gasoline VOC Storage Tanks	
IEU14	Sewer Manholes, Junction Boxes, Sumps and Lifts Associated with Wastewater Treatment	
IEU15	Fugitive Emissions: Diesel Fuel & Gasoline Fuel Combustion	
IEU16	Feedwater Treatment Unit/Pumphouse	
IEU17	Adsorber (AT-1) System (Flare Gas Treatment Unit)	
IEU18	65,000 Gallon Amine Storage Bullets (Flare Gas Treatment Unit)	
IEU19	Cooling Tower	
IEU20	Boiler Blowdown Tank	
IEU21	Flare Gas Water Seal System	
IEU22	Flare Gas Total Sulfur Analyzer	

SECTION III. PERMIT CONDITIONS

A. Emission Limits and Standards

The rule citations for all emission limits are included in the operating permit. In addition to those previously listed in the operating permit, the Department included the requirements of the Federal Implementation Plan for the Billings/Laurel, Montana, Sulfur Dioxide Area. Otherwise, there are no emission limits or standards identified in this permit that were not previously applicable to the facility either by rule, permit or by the Board of Environmental Review (Board) Order signed on June 12, 1998.

Opacity

This permit contains requirements for MSCC to perform semiannual Method 9 tests for both the 30-Meter and 100-Meter stacks. All major emission units are vented to these stacks as well as individual stacks. For those individual stacks, a Method 9 shall be performed upon request of the Department. The compliance demonstrations for the individual stacks require that all fuel burning units fire either natural or low sulfur refinery fuel gas when venting to individual stacks; thus, opacity limitations should not be violated when emissions units are operating.

For those non-fuel burning process emission units Method 9 tests will be required as requested by the Department. For those emission units that have a remote chance of violating opacity limits have, the permit does not include any testing requirements. Those units include EU16 Liquid Hydrogen Sulfide (H₂S) and Compressor Unit; (2); EU17 Molten Sulfur Storage; EU17.a Molten Sulfur Storage in Railcars and Mobile Tanks; EU18 Molten Sulfur Loadout/Unloading; EU19 Molten Sulfur Run-down Pits; EU22 Various Valve, Pump and Flange Leaks, EU20 Sulfur and Fertilizer Manufacture, Conveying and Loadout; and EU21 Sulfur Product Manufacture, Conveying and Loadout.

Particulate Matter - Industrial Processes and Fuel Burning Equipment

This permit does not require any specified Method 5 testing because this facility does not have any particulate emission limits established other than those applicable to process weight and fuel burning equipment. Furthermore, the SIP, Board Order signed on January 25, 1978, specifies how process weight is to be interpreted and it is highly unlikely that any process would violate either process weight or the particulate fuel burning limitations when only natural gas or low sulfur refinery fuel gas is burned. Thus, testing will only be required as requested by the Department.

SO₂ Emission Limits

MSCC has established emission limits for the 100-Meter Stack, the 30-Meter Stack, and boiler specific stacks. For cases, where the emission units are vented to the 100-Meter stack, a SO₂ CEMs and annual testing (Method 6/6C) shall be used to demonstrate compliance with the emission limits.

For other fuel burning emissions units, the permit has included emission limits for the 30-Meter stack and a collective emission limit for boilers when exhausting to individual or auxiliary stacks.

TRD2611-06 20 Date of Decision: 3/22/2019 Effective Date: 4/23/2019 In this case, the compliance demonstration method requires that MSCC burn only natural gas, or perform Draeger Tube testing (or equivalent as approved by the Department) in coordination with recording the refinery fuel gas consumption to demonstrate compliance with the 12 lb/3hr SO₂ limit. By demonstrating compliance with the 12 lb/3 hr SO₂ limit, MSCC is presumed to be in compliance with the sulfur in fuel limits.

As stated above, the compliance demonstrations established by this permit for those sources not venting to the 100-Meter Stack requires that MSCC burn only natural gas, or perform a Draeger Tube testing (or equivalent) in order to assure compliance for those sources that burn refinery fuel gas.

NO_x Emission Limits

The only NO_x limits included in this permit are for the Monaca Heaters and Hydrogen Plant. The potential emissions from these sources are less than the trigger level for testing according to Departmental policy. Therefore, these units will only be tested as deemed necessary by the Department.

В. **Monitoring Requirements**

ARM 17.8.1212(1) requires that all monitoring and analysis procedures or test methods required under applicable requirements are contained in operating permits. In addition, when the applicable requirement does not require periodic testing or monitoring, periodic monitoring must be prescribed that is sufficient to yield reliable data from the relevant time period that is representative of the source's compliance with the permit.

The requirements for testing, monitoring, recordkeeping, reporting, and compliance certification sufficient to assure compliance do not require the permit to impose the same level of rigor for all emissions units. Furthermore, they do not require extensive testing or monitoring to assure compliance with the applicable requirements for emission units that do not have significant potential to violate emission limitations or other requirements under normal operating conditions. When compliance with the underlying applicable requirement for a insignificant emissions unit is not threatened by lack of regular monitoring and when periodic testing or monitoring is not otherwise required by the applicable requirement, the status quo (i.e., no monitoring) will meet the requirements of ARM 17.8.1212(1). Therefore, the permit does not include monitoring for insignificant emission units.

The permit includes periodic monitoring or recordkeeping for each applicable requirement. The information obtained from the monitoring and recordkeeping will be used by the permittee to periodically certify compliance with the emission limits and standards. However, the Department may request additional testing to determine compliance with the emission limits and standards.

C. Test Methods and Procedures

The operating permit may not require testing for all sources if routine monitoring is used to determine compliance, but the Department has the authority to require testing if deemed necessary to determine compliance with an emission limit or standard. In addition, the permittee may elect to voluntarily conduct compliance testing to confirm its compliance status.

D. Recordkeeping Requirements

The permittee is required to keep all records listed in the operating permit as a permanent business record for at least five-years following the date of the generation of the record.

E. **Reporting Requirements**

Reporting requirements are included in the permit for each emissions unit and Section V of the operating permit "General Conditions" explains the reporting requirements. However, the permittee is required to submit semi-annual and annual monitoring reports to the Department and to annually certify compliance with the applicable requirements contained in the permit. The reports must include a list of all emission limit and monitoring deviations, the reason for any deviation, and the corrective action taken as a result of any deviation.

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SECTION IV. NON-APPLICABLE REQUIREMENTS

Pursuant to ARM 17.8.1221, MSCC requested a permit shield for all non-applicable regulatory requirements and regulatory orders identified in the tables in Section 8 of the permit application. In addition, the MSCC permit application identified a permit shield request for applicable requirements for both the facility and for certain emission units.

The following table outlines those requirements that MSCC had identified as non-applicable but, after Department review, will not be included in the operating permit as non-applicable. The table includes both the applicable requirement and reason that the Department did not identify this requirement as non-applicable.

Requirements Not Included in Section IV. Non-applicable Requirements of the Operating **Permit**

Rule Citation		D
State	Federal	Reason
	40 CFR 51 40 CFR 52 40 CFR 53 40 CFR 54 40 CFR 56 40 CFR 58	Although these rules contain requirements for the regulatory authorities and not major sources, these rules can be used as authority to impose specific requirements on a major source.
	40 CFR 60, Subpart A 40 CFR 61, Subpart A 40 CFR 62 40 CFR 63, Subparts A-F	Although these rules contain requirements for the regulatory authorities and not major sources, these rules can be used as authority to impose specific requirements on a major source.
	40 CFR 64 40 CFR 66 40 CFR 67	Although these rules contain requirements for the regulatory authorities and not major sources, these rules can be used as authority to impose specific requirements on a major source.
	40 CFR 70 – 71	Although these rules contain requirements for the regulatory authorities and not major sources, these rules can be used as authority to impose specific requirements on a major source.
	40 CFR 72 - 78	The facility is not in this source category.
	40 CFR 81	Although these rules contain requirements for the regulatory authorities and not major sources, these rules can be used as authority to impose specific

	Rule Citation	P
State	Federal	Reason
		requirements on a major source.
	40 CFR 82 (Except subparts B&F).	This rule refers to a process, equipment, or activity that is not used at this facility.
ARM 17.8.101 ARM 17.8.102 ARM 17.8.103 ARM 17.8.301 ARM 17.8.302 ARM 17.8.401 ARM 17.8.501 ARM 17.8.601 ARM 17.8.602 ARM17.8.740 ARM 17.8.801 ARM 17.8.802 ARM 17.8.901 ARM 17.8.902 ARM 17.8.1001 ARM 17.8.1001 ARM 17.8.1002 ARM 17.8.1101 ARM 17.8.1101 ARM 17.8.1101 ARM 17.8.1101 ARM 17.8.1102 ARM 17.8.1103 ARM 17.8.1201 ARM 17.8.1201 ARM 17.8.1203 ARM 17.8.1234		Rules that consist of either a statement or of purpose, applicability statement, regulatory definitions or a statement of incorporation by reference. These types of rules do not have specific requirements associated with them.
ARM 17.8.120 ARM 17.8.121 ARM 17.8.131		Rules that do not have specific requirements that may become relevant to a major source during the permit span.
ARM 17.8.140 ARM 17.8.141 ARM 17.8.511 ARM 17.8.514 ARM 17.8.611 ARM 17.8.612 ARM 17.8.613 ARM 17.8.615 ARM 17.8.615 ARM 17.8.804 ARM 17.8.805 ARM 17.8.905 ARM 17.8.906		Procedural rules that have specific requirements that may become relevant to a major source during the permit span.

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Rule Cita	Paggar	
State	Federal	Reason
ARM 17.8.1005		
ARM 17.8.1006		
ARM 17.8.1007		
ARM 17.8.1224		
ARM 17.8.1226		
ARM 17.8.1227		
ARM 17.8.SubChapter 14		
ARM 17.8.142		
ARM 17.8.510		
ARM 17.8.806		
ARM 17.8.807		
ARM 17.8.808		Rules that do not have specific
ARM 17.8.1108		requirements for major sources
ARM 17.8.1109		because they are requirements for
ARM 17.8.1210		EPA or state and local authorities
ARM 17.8.1211		and should never be shielded.
ARM 17.8.1212		Note: Although these rules
ARM 17.8.1213		contain requirements for the
ARM 17.8.1214		regulatory authorities and not
ARM 17.8.1215		major sources, these rules can be
ARM 17.8.1222		used as authority to impose
ARM 17.8.1223		specific requirements on a major
ARM 17.8.1225		source.
ARM 17.8.1228		
ARM 17.8.1231		
ARM 17.8.1232		
ARM 17.8.1233		
ARM 17.8.326		Rules that are always applicable to a major source and may contain specific requirements for compliance.
ARM 17.8.330		Rules that consist of either a statement of purpose, applicability statement, regulatory definitions or a statement of incorporation by reference. These types of rules do not have specific requirements associated with them.

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SECTION V. FUTURE PERMIT CONSIDERATIONS

A. **MACT Standards**

As of the issuance date of Operating Permit #OP2611-06, the only MACTs that the Department is aware which MSCC may be subject to Subpart ZZZZ National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines, Subpart CCCCCC National Emission Standards for Hazardous Air Pollutants for Source Category: Gasoline Dispensing Facilities, and Subpart [][]] - National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers Area Sources.

В. **NESHAP Standards**

As of the issuance date of Operating Permit #OP2611-06, the Department is unaware of any future requirement that may be promulgated during the permit term for which this facility must comply.

C. **NSPS Standards**

As of the issuance date of Operating Permit #OP2611-06, the Department is unaware of any future NSPS requirement that may be promulgated that would affect this facility. The only NSPS requirements that the facility may be subject to include 40 CFR 60, Subparts D, Da, Db, and Dc Standards of Performance for Industrial-Commercial-Institutional Steam Generating Units, and 40 CFR 60, Subpart J Standards of Performance for Petroleum Refineries. However, these subparts are not applicable to this facility for the following reasons.

40 CFR 60, Subpart I is not applicable because MSCC is not an "affected facility" as defined by this subpart for either fuel gas combustion or the Claus plant. The Claus plant was constructed in approximately 1955, which is before the applicability date for this NSPS. In addition, fuel gas combustion devices are not an "affected facility" under this NSPS because the fuel is not combusted within a "refinery" and it precedes the date of applicability for this NSPS, which is June 11, 1973.

In addition Subpart D, Da, Db, or Dc is not applicable for this facility because none of the boilers located at the facility meet either the size or applicability dates contained in the definition of affected facilities.

D. Risk Management Plan

MSCC was previously subject to this because they stored H₂S and carbon disulfide in greater quantities than the minimum threshold quantity defined by 40 CFR §68.115 or 40 CFR \$68.130. However, in review of the existing processes the quantity of materials at the facility fell below the threshold and MSCC no longer meets the applicability requirements of 40 CFR Part 68.10. Notification of this was submitted to the EPA on May 22, 2007.

E. CAM Applicability

For purposes of CAM, a control device does not include passive control measures that act to prevent pollutants from forming, such as the use of seals, lids, or roofs to prevent the release of pollutants, the use of low-polluting fuel or feedstocks, the use of combustion or other process design features or characteristics, or inherent process equipment. As such, MSCC's equipment would not be considered control equipment as it is inherent part of the process. It was determined that MSCC does not have a unit with potential pre-control device emissions of the applicable regulated air pollutant that are equal to or greater than 100 percent of the amount, in tons per year, required for a source to be classified as a major (Part 70) source.

F. PSD and Title V Greenhouse Gas Tailoring Rule

On May 7, 2010, EPA published the "light duty vehicle rule" (Docket # EPA-HQ-OAR-2009-0472, 75 FR 25324) controlling greenhouse gas (GHG) emissions from mobile sources, whereby GHG became a pollutant subject to regulation under the Federal and Montana Clean Air Act(s). On June 3, 2010, EPA promulgated the GHG "Tailoring Rule" (Docket # EPA-HQ-OAR-2009-0517, 75 FR 31514) which modified 40 CFR Parts 51, 52, 70, and 71 to specify which facilities are subject to GHG permitting requirements and when such facilities become subject to regulation for GHG under the PSD and Title V programs.

Under the Tailoring Rule, any PSD action (either a new major stationary source or a major modification at a major stationary source) taken for a pollutant or pollutants other than GHG that would become final on or after January 2, 2011 would be subject to PSD permitting requirements for GHG if the GHG increases associated with that action were at or above 75,000 TPY of carbon dioxide equivalent (CO₂e) and greater than 0 TPY on a mass basis. Similarly, if such action were taken, any resulting requirements would be subject to inclusion in the Title V Operating Permit. Facilities which hold Title V permits due to criteria pollutant emissions over 100 TPY would need to incorporate any GHG applicable requirements into their operating permits for any Title V action that would have a final decision occurring on or after January 2, 2011.

Starting on July 1, 2011, PSD permitting requirements would be triggered for modifications that were determined to be major under PSD based on GHG emissions alone, even if no other pollutant triggered a major modification. In addition, sources that are not considered PSD major sources based on criteria pollutant emissions would become subject to PSD review if their facility-wide potential emissions equaled or exceeded 100,000 TPY of CO₂e and 100 or 250 TPY of GHG on a mass basis depending on their listed status in ARM 17.8.801(22) and they undertook a permitting action with increases of 75,000 TPY or more of CO₂e and greater than 0 TPY of GHG on a mass basis. With respect to Title V, sources not currently holding a Title V permit that have potential facility-wide emissions equal to or exceeding 100,000 TPY of CO₂e and 100 TPY of GHG on a mass basis would be required to obtain a Title V Operating Permit.

Date of Decision: 3/22/2019 Effective Date: 4/23/2019 The Supreme Court of the United States (SCOTUS), in its Utility Air Regulatory Group v. EPA decision on June 23, 2014, ruled that the Clean Air Act neither compels nor permits EPA to require a source to obtain a PSD or Title V permit on the sole basis of its potential emissions of GHG. SCOTUS also ruled that EPA lacked the authority to tailor the Clean Air Act's unambiguous numerical thresholds of 100 or 250 TPY to accommodate a CO2e threshold of 100,000 TPY. SCOTUS upheld that EPA reasonably interpreted the Clean Air Act to require sources that would need PSD permits based on their emission of conventional pollutants to comply with BACT for GHG. As such, the Tailoring Rule has been rendered invalid and sources cannot become subject to PSD or Title V regulations based on GHG emissions alone. Sources that must undergo PSD permitting due to pollutant emissions other than GHG may still be required to comply with BACT for GHG emissions.

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